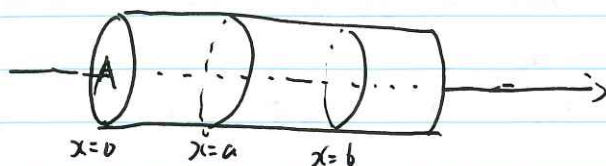


Heat equation.

Consider a 1D rod of length L



We want to derive an equation that governs the temperature distribution inside the rod.

First, we define a quantity $e(x,t)$ called thermal energy density which describes the amount of thermal energy per unit volume.

Denote by A the cross-sectional area of the rod and assume A is const.

Q1: What is the total thermal energy of the rod between $x=a$ and $x=b$?

$$\int_a^b e(x,t) A dx$$

Q2: How can the total thermal energy be changed?
We assume that the lateral surface to be insulated.

Conservation of heat energy:

$$\boxed{\text{rate of change of heat energy in time}} = \boxed{\text{heat energy flowing across boundaries per unit time}} + \boxed{\text{heat energy generated inside per unit time}}$$

Define: $\Phi(x,t)$ = amount of thermal energy per unit time that flows to the right per unit surface area

We call $\phi(x,t)$ the heat flux.

Q3: What does $\phi(x,t) < 0$ mean?

Defn: $Q(x,t)$: heat energy per unit volume generated per unit time.

We call $Q(x,t)$ the heat sources.

Now, in equation, the conservation of heat energy reads.

$$\frac{d}{dt} \int_a^b e(x,t) A dx = \phi(a,t) A - \phi(b,t) A + A \int_a^b Q(x,t) dx$$

Q4: Why on the LHS of the equation we ~~not~~ use the ordinary differentiation $\frac{d}{dt}$ rather than $\frac{\partial}{\partial t}$?

Suppose $e(x,t)$ is differentiable.

$$\frac{d}{dt} \int_a^b e dx = \int_a^b \frac{\partial e}{\partial t} dx$$

If $\phi(x,t)$ is continuously differentiable, by the Fundamental theorem of calculus.

$$\phi(a,t) A - \phi(b,t) A = -A \int_a^b \frac{\partial \phi}{\partial x} dx$$

Hence, after dividing both sides and rearranging the terms

$$\int_a^b \left[\frac{\partial e}{\partial t} + \frac{\partial \phi}{\partial x} - Q \right] dx = 0 \Rightarrow \text{integral conservation law.}$$

Since this holds for arbitrary a, b , $\left[\frac{\partial e}{\partial t} + \frac{\partial \phi}{\partial x} - Q \right]$ must be zero.

Q5: Explain in detail why this is true? What happens if the integrand is not zero at somewhere?

Now we also have the differential conservation form

$$\frac{\partial e}{\partial t} + \frac{\partial \phi}{\partial x} - Q = 0$$

Suppose now $Q = 0$.

If $\frac{\partial \phi}{\partial x} > 0 \Rightarrow \phi$ increases with $x \Rightarrow \phi(a, t) < \phi(b, t)$

$\Rightarrow \frac{\partial e}{\partial t} = -\frac{\partial \phi}{\partial x} < 0 \Rightarrow e(x, t)$ will decrease in time.

Next, we want to look at the relation between thermal energy $e(x, t)$ and the temperature $u(x, t)$.

Defn

$c(x)$, ~~$c(x)$~~ = heat capacity (the heat energy that must be supplied to a unit mass of a substance to raise its temperature one unit).

$\rho(x)$ = mass density (mass per unit volume).

~~Plug in the~~ The total mass of a thin slice is $\rho A \Delta x$, and hence the total thermal energy in ~ this slice is $c(x) u(x, t) \rho A \Delta x$.

$$\text{Therefore } e(x, t) A \Delta x = c(x) u(x, t) \rho A \Delta x$$

$$\Rightarrow e(x, t) = c(x) \rho(x) u(x, t)$$

Plug this into the differential law of conservation.

$$c(x) \rho(x) \frac{\partial u}{\partial t} = -\frac{\partial \phi}{\partial x} + Q \quad (*)$$

Fourier's law of heat conduction

1. If the temperature is the same everywhere, there is no heat flow

2. If there is temperature variation, then heat flows from hot area to the cold area.
3. The greater the temperature difference, the greater heat flow.
4. Heat flow also depends on materials.

Fourier's law : $\phi = -K_0 \frac{\partial u}{\partial x}$

which asserts that the heat flux is proportional to the temperature difference, where $K_0 = K_0(x)$ is the thermal conductivity which measures the ability of the material to conduct heat.

Q6: Explain why there is a minus sign?

Suppose $\frac{\partial u}{\partial x} > 0 \Rightarrow u$ increases as x increases, hence $u(a,t) < u(b,t)$ and heat will flow from right to the left.

Now we are ready to derive the heat equation in 1D.

Put the Fourier's law in eqn (x).

$$c\rho \frac{\partial u}{\partial t} = -\frac{\partial}{\partial x} \left(-K_0 \frac{\partial u}{\partial x} \right) + Q$$

$$= \frac{\partial}{\partial x} \left(K_0 \frac{\partial u}{\partial x} \right) + Q$$

In some special cases, c, ρ, K_0 are constants, we can further simplify the above equation.

$$c\rho \frac{\partial u}{\partial t} = K_0 \frac{\partial^2 u}{\partial x^2} + Q$$

I) in addition, there are no sources, $Q=0$

$$\Rightarrow \frac{\partial u}{\partial t} = k \frac{\partial^2 u}{\partial x^2} \quad (**) \quad \text{where } k = \frac{K_0}{c\rho}$$

is called the thermal diffusivity.
 Eqn. (***) is called the heat equation, which corresponds to no sources and constant thermal properties.

Initial / Boundary conditions.

Initial condition (IC) for heat equations
 $u(x, 0) = f(x)$.

In order to predict the future temperature, only knowing initial condition is not enough. We need boundary conditions (BC) as well.

Q7: How many boundary condition do we need for heat equations?

There are 3 types of boundary conditions (BC).

1. Dirichlet BC : prescribed temperature.

For example at $x=0$, $u(0, t) = U_B(t)$, where $U_B(t)$ is a given temperature of surrounding medium.

2. Neumann BC: prescribed gradient / flux (Insulated boundary).

Eq. $-K_0(0) \frac{\partial u}{\partial x} \Big|_{x=0} = \phi(t)$ where $\phi(t)$ is given.

↑
 heat flux at $x=0$. If $\phi(t) = 0 \Rightarrow$ no heat flux / perfectly insulated.

3. Mixed BC: Newton's law of cooling

Eq. At $x=0$.

$-K_0(0) \frac{\partial u}{\partial x} \Big|_{x=0} = -H [u(0, t) - U_B(t)]$.

↑
 heat flux
 difference of temperature of the rod at $x=0$ and temperature U_B of the surrounding medium.

Here $H > 0$: convection coefficient / heat transfer coefficient.

$$\text{at } x = L \quad -k_0(L) \frac{\partial u}{\partial x} \Big|_{x=L} = H [u(L, t) - U_B(t)].$$

Q.8: Why the RHS of two boundary conditions should have different signs?

Remark: if $H \neq 0$, then this BC models non-perfectly insulated boundary, which means the heat is lost or gained through the boundary $u(x, t) \rightarrow U_B(t)$.